Surface Areas and Catalytic Activities of Mn-substituted Hexaaluminates with Various Cation Compositions in the Mirror Plane

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Surface areas and catalytic activities of Mn-substituted hexaaluminates were investigated as a function of cation composition in the mirror plane. After calcination at 1300 °C, the surface areas of  $\text{Ba}_{1-x} \text{K}_x \text{MnAl}_{11} \text{O}_{19-\alpha}$  and  $\text{Sr}_{1-x} \text{La}_x \text{MnAl}_{11} \text{O}_{19-\alpha}$  increased with x and attained to be above 23 m²/g at the optimum compositions. The methane combustion activities of these oxides were higher than those of 1 wt% Pt/Al<sub>2</sub>O<sub>3</sub> and LaCoO<sub>3</sub>.

Polycrystalline barium hexaaluminate as well as other "layered" hexaaluminates is known to maintain large surface areas at higher temperatures,  $^{1-3)}$  which are quite adequate for catalysts of high temperature combustion.  $^{4,5)}$  In particular, the samples prepared by hydrolysis of metal alkoxides retain surface area of more than 10 m²/g after calcination at 1600 °C for 5 h.  $^{6)}$  As reported previously,  $^{7,8)}$  various elements are incorporated in the layered hexaaluminate lattice by partial replacement of Al³+ cations in BaAl $_{12}O_{19}$ . When the amount of substituent is small enough not to destroy the large surface area, the manganese-system (BaMnAl $_{11}O_{19-\alpha}$ ) was the most active among transition metal substituted hexaaluminates. However, the catalytic activity of BaMnAl $_{11}O_{19-\alpha}$  was not satisfactory to be used as a high temperature combustion catalyst. In this communication, we report the enhancement of the catalytic properties and surface areas of Mn-substituted hexaaluminates (A $_{1-x}$ A' $_x$ MnAl $_{11}O_{19-\alpha}$ ) by controlling the cation composition in the mirror plane, x.

Cation-substituted hexaaluminates were prepared by hydrolysis of composite alkoxides as previously described. Calculated amounts of  $Ba(OC_3H_7)_2$ ,  $Sr(OC_3H_7)_2$ ,  $Ca(OC_3H_7)_2$ ,  $La(OC_3H_7)_3$ , and/or  $Al(OC_3H_7)_3$  were dissolved in 2-propanol. An aqueous solution of manganese nitrate and potassium nitrate was added into the 2-propanol solution of alkoxides. The resulting hydrolyzed gel was thermally decomposed at 500 °C and subsequently calcined at 1300 °C in air. Crystal structure and surface area were determined by X-ray diffraction and the BET method, respectively. Catalytic combustion of methane was carried out in a flow system as described elsewhere. 3)

A series of hexaaluminates are comprised of stacking of close-packed oxygen ion layers (spinel blocks) which are separated each other by a monoatomic layer (mirror plane). The crystal structure of hexaaluminate is  $\beta$ -alumina (AAl<sub>11</sub>O<sub>17</sub>) or magnetoplumbite type (AAl<sub>12</sub>O<sub>19</sub>), depending on an ionic radius and a valence of the large cation (A-site) in the mirror plane.  $^{9}$ )  $\beta$ -Alumina structure can be

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Table 1. Phases, surface areas, and catalytic activities of Mn-substituted hexaaluminates with various cation compositions in the mirror plane

Composition	r <sub>M</sub> a)	Surface area m <sup>2</sup> g <sup>-1</sup>	Catalytic activity T <sub>10%</sub> /°C <sup>b)</sup>	Crystalline phase <sup>c)</sup>
$BaMnAl_{11}O_{19-\alpha}$	-	13.7	540	<sup>BA</sup> 6
$^{\text{Ba}}_{0.8}^{\text{K}}_{0.2}^{\text{MnAl}}_{11}^{0}_{19-\alpha}$	0.98	23.3	505	<sup>BA</sup> 6
Ba <sub>0.8</sub> La <sub>0.2</sub> MnAl <sub>11</sub> O <sub>19-0</sub>	ν 0.84	12.0	550	$^{\mathrm{BA}}$ 6 + $^{\alpha}$
Ba <sub>0.6</sub> Sr <sub>0.2</sub> MnAl <sub>11</sub> O <sub>19-6</sub>	0.85	15.1	535	<sup>BA</sup> 6
SrMnAl <sub>11</sub> O <sub>19-α</sub>	_	13.4	540	quasi-SA <sub>6</sub>
Sr <sub>0.8</sub> La <sub>0.2</sub> MnAl <sub>11</sub> O <sub>19-0</sub>	0.98	23.8	500	sa <sub>6</sub>
Sr <sub>0.8</sub> K <sub>0.2</sub> MnAl <sub>11</sub> O <sub>19-α</sub>	0.87	12.9	550	quasi-SA <sub>6</sub>
Sr <sub>0.8</sub> Ca <sub>0.2</sub> MnAl <sub>11</sub> O <sub>19-0</sub>	0.86	7.3	550	quasi-SA <sub>6</sub>
$CaMnAl_{11}O_{19-\alpha}$	-	4.0	565	CA <sub>6</sub> + CA <sub>2</sub>

All samples were calcined at 1300 °C for 5 h. a) Ratio of ionic radii between A and A' of  $^{A}$ 0.2 MnAl<sub>11</sub>0<sub>19- $^{\alpha}$ </sub> b) Temperature at which conversion level is  $^{10}$ 8. Reaction condition:  $^{CH}$ 4 1 vol8, air 99 vol8, S.V. =  $^{48000}$ 6 h<sup>-1</sup> c)  $^{BA}$ 6 =  $^{BaAl}$ 120<sub>19</sub>,  $^{CA}$ 6 =  $^{CaAl}$ 120<sub>19</sub>,  $^{CA}$ 6 =  $^{CaAl}$ 120<sub>19</sub>,  $^{CA}$ 9 Ca<sub>2</sub> =  $^{CaAl}$ 40<sub>7</sub>,  $^{\alpha}$ 8 =  $^{\alpha}$ -Al<sub>2</sub>0<sub>3</sub>

obtained for the hexaaluminates with alkaline elements and Ba, while magnetoplumbite structure for those with other alkaline earth and some rare earth elements. Crystalline phases, surface areas, and catalytic activities of Mnsubstituted hexaaluminates with various compositions of mirror plane cations are investigated as summarized in Table 1. The crystal structure of  $BaMnAl_{11}O_{19-\alpha}$  as well as BaAl<sub>12</sub>O<sub>19</sub> was the hexagonal layered hexaaluminate type, whereas that of  ${\tt SrMnAl}_{11}{\tt O}_{19-lpha}$  was deteriorated to monoclinic. These two samples, consisting of the single phases, possessed large surface areas (13  $m^2/g$ ). The CaMnAl<sub>11</sub>O<sub>19- $\alpha$ </sub> sample decomposed into CaAl<sub>12</sub>O<sub>19</sub> and CaAl<sub>4</sub>O<sub>7</sub> phases. The precipitation of the second phase always results in low surface area.

Substituents A' in  $A_{0.8}A'_{0.2}MnAl_{11}O_{19-\alpha}$  are chosen to minimize the deviation of an ionic radius from that of the host cation. Thus, the ratio of ionic radii between A and A'  $(r_{M})$  is defined as shown in Table 1. Potassium cations occupied the Ba sites without any phase separation after calcination at 1300 °C. Both surface area and catalytic activity were enhanced by substitution of K for Ba. The catalytic activity was also promoted by Sr-substitution for La (Sr<sub>0.8</sub>La<sub>0.2</sub>- $\text{MnAl}_{11}\text{O}_{19-\alpha}$ ) in which a single hexaaluminate phase attained the surface area of 24 m<sup>2</sup>/g. Other combinations of mirror plane cations were not effective in improving surface area or catalytic activity. It is noted that the combination of different mirror plane cations enhances the catalyst performance and the surface area of Mn-substituted hexaaluminates, only when the size of substituent is close to that of host cation  $(r_M = 1)$ .

Further investigation was focused on the two Mn-substituted hexaaluminates,  $Ba_{1-x}K_xMnAl_{11}O_{19-\alpha}$  and  $Sr_{1-x}La_xMnAl_{11}O_{19-\alpha}$ , in which large surface area and high catalytic activity are simultaneously attained. Figure 1 shows the surface areas of the two systems after calcination at 1300 °C as a function of composition, x. The surface  $Ba_{1-x}K_xMnAl_{11}O_{19-\alpha}$  increased monotonously with K-substitution  $26 \text{ m}^2/\text{g}$  at  $x = 1.0 \text{ (KMnAl}_{11}O_{19-\alpha})$ . this system The surface area of obviously relates to K content in the mirror plane. Sr-substitution for La also gave rise to the maximum surface area at  $x = 0.2 (23 \text{ m}^2/\text{g})$ . for the effect explanation substitution on the surface area is unclear at present, but is likely related to the crystalline morphology. Transmission electron microscopic observation indicated that crystal growth along the c axis (normal to the mirror plane) is strongly suppressed in the present system. Substitution of mirror plane cations is expected to modify the interlayer distance of spinel aluminate layers stacking rate along the c axis.

Figure 2 shows the activities for methane combustion over  $Ba_{1-x}K_xMnAl_{11}O_{19-\alpha}$ and Sr<sub>1-x</sub>La<sub>x</sub>-MnAl<sub>11</sub>O<sub>19-α</sub>• The activities expressed as ignition temperatures, at which conversion T<sub>10%</sub>, attained to be 10%. The ignition temperatures  $(T_{10})$  of the two systems were lowered with increasing x maximum activities obtained were at x = 0.2. The change in T<sub>10%</sub> very small for  $Ba_{1-x}K_xMnAl_{11}O_{19-\alpha}$  at  $x \rightarrow 0.2$ ; however, the content of K should be low to avoid volatilization at high temperatures.

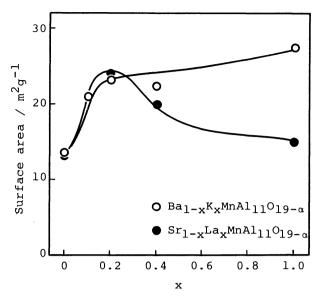


Fig. 1. Surface areas of cation-substituted hexaaluminates after calcination at 1300 °C.

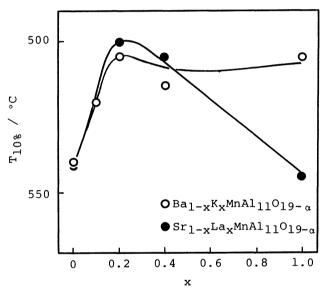


Fig. 2. Methane combustion activities of cation-substituted hexaalumi-nates after calcination at 1300 °C.

 $\rm T_{10\,\%}$  denotes the temperature at which conversion level of methane is 10%.

Reaction conditions : see Table 1.

The behavior of catalytic activity corresponds well to that of the surface area in Fig. 1.

The catalytic activities of Mn-substituted hexaaluminates were compared with combustion catalysts so far used popularly, i.e.,  $LaCoO_3$  and 1 wt%  $Pt/Al_2O_3$  (Fig. 3). After calcination at 1300 °C, combustion activities of the conventional catalysts were significantly lowered because of decreases in surface area. The energy dispersive X-ray analysis of  $Pt/Al_2O_3$  revealed that ca. 10% of platinum

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loading was eliminated during calcination at 1300 °C for 5 h. In contrast, the large surface area of the cation-substituted hexaaluminates leads to high combustion activity even at low Mn content. The catalytic activities of two cation substituted hexaaluminate samples were the same as or higher than those of LaCoO3 and Pt/Al2O3 in the whole temperature range. Since the activities per unit surface area of LaCoO, and Pt/Al<sub>2</sub>O, are expected to be higher than those of the cation-substituted hexaaluminates, the large surface area of the latter samples are attaining effective in combustion activities, especially under high flow rate conditions  $(S.V. > 10^5 h^{-1})$  as in a gas turbine combustor. Thus, characteristic feature

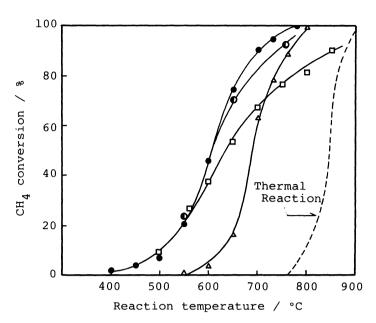


Fig. 3. Catalytic combustion over various catalysts after calcination at 1300 °C.

Catalyst	Surface area/m <sup>2</sup> g <sup>-1</sup>
• Sr <sub>0.8</sub> La <sub>0.2</sub> MnAl <sub>11</sub> O <sub>1</sub>	$9-\alpha$ 23.8
● Ba <sub>0.8</sub> K <sub>0.2</sub> MnAl <sub>11</sub> O <sub>19</sub> □ LaCoO <sub>3</sub>	$\frac{1-\alpha}{0.3}$ 23.3
△ lwt%Pt/Al <sub>2</sub> O <sub>3</sub>	1.5

Reaction conditions : see Table 1.

hexaaluminate catalysts is the high resistances against thermal deactivation and sintering, which result from 1) high heat resistance of hexaaluminate matrix, 2) the catalytic activity of Mn species, and 3) the mirror plane cations which stabilize large surface area.

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